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Instructions : (1) All Questions are compulsory.
(2) Answer each next main Question on a new page.
(3) Illustrate your answers with neat sketches wherever necessary.
(4) Figures to the right indicate full marks.
(5) Use of Non-programmable Electronic Pocket Calculator is permissible.
(6) Mobile Phone, Pager and any other Electronic Communication devices are not permissible in Examination Hall.

## Marks

1. (A) Attempt any FOUR of the following :
(i) State Henry's law \& Raoult's law.
(ii) Define limiting reactant \& excess reactant.
(iii) Define standard heat of formation and standard heat of combustion.
(iv) What is Recycling operation? State one purpose of recycling operation.
(v) Define partial pressure and pure component volume.
(vi) The carbon monoxide is reacted with hydrogen to produce methanol.
(B) Attempt any TWO of the following:
(i) A mixture of phenol \& water forms two separate liquid phases, one rich in phenol and other rich in water, composition of layers is $70 \%$ and $9 \%$ (by weight) phenol resp. If 500 kg of phenol \& 700 kg of water are mixed and layers allowed to separate, what will be the weights of two layers?
(ii) Calculate the numbers of cubic metres of acetylene gas at a temperature of $313{ }^{\circ} \mathrm{k}$ and pressure of 100 kPa that may be produced from 5 kg of calcium carbide.
(iii) $\mathrm{SO}_{2}$ is oxidised to $\mathrm{SO}_{3}$. If the conversion is $70 \%$ and air is used in $80 \%$ excess than theoretical requirement.

Calculate : (a) kmol of air fed per kmol of $\mathrm{SO}_{2}$, (b) Composition of gases leaving the reactor on mole basis.

## 2. Attempt any FOUR :

(i) A combustion reactor is fed with $50 \mathrm{kmol} / \mathrm{h}$ of butane and $2100 \mathrm{kmol} / \mathrm{h}$ of air. Calculate the \% excess of air used.
(ii) State and explain Hess's law of constant heat summation.
(iii) It is desired to make up 1000 kg of solution containing $35 \%$ by weight of substance ' A '.

Two solutions are available, one containing $10 \%$ by weight A and other containing $50 \%$ by weight A .

How many kilograms of each solution will be required?
(iv) Tray dryer is fed with 1000 kg of wet orthonitro aniline (ONA) containing $10 \%$ water. The dried product contains $99.5 \%$ ONA and rest water.

Calculate the percentage of original water removed in dryer.
(v) A mixture of $\mathrm{CH}_{4}$ and $\mathrm{C}_{2} \mathrm{H}_{6}$ has the average molecular weight of 22.4. Find the $\mathrm{mol} \%$ of $\mathrm{CH}_{4} \& \mathrm{C}_{2} \mathrm{H}_{6}$ in mixture.
(vi) A feed containing A, B and inert enters a reactor. The reaction taking place is $2 \mathrm{~A}+\mathrm{B} \rightarrow \mathrm{C}$. The product leaving the reactor contains $23.08 \% \mathrm{~A}, 11.54 \% \mathrm{~B}$, $46.15 \% \mathrm{C}$ and $19.23 \%$ inert (by mole). Find the analysis of feed on mole basis.

## 3. Attempt any TWO of the following :

(i) In the manufacture of chlorine, feed containing hydrochloric acid gas and air are fed to an oxidiser. The product gases leaving the oxidiser are found to contain $13.2 \% \mathrm{HCl}, 6.3 \% \mathrm{O}_{2}, 42.9 \% \mathrm{~N}_{2}, 30 \% \mathrm{Cl}_{2}$ and $7.6 \% \mathrm{H}_{2} \mathrm{O}$ (by weight). Calculate : (a) The percent excess air used. (b) Composition of gas mixture entering the oxidiser, by weight.
(ii) A stream flowing at a rate of $15000 \mathrm{~mol} / \mathrm{h}$ containing $25 \mathrm{~mol} \% \mathrm{~N}_{2} \& 75 \mathrm{~mole}$ $\% \mathrm{H}_{2}$ is to be heated from $29{ }^{\circ} \mathrm{K}$ to $473^{\circ} \mathrm{K}$.

Calculate the heat that must be transferred, using $\mathrm{C}_{\mathrm{p}}{ }^{\circ}$ data given below :

$$
\mathrm{C}_{\mathrm{p}}^{\circ}=\mathrm{a}+\mathrm{bT}+\mathrm{cT}^{2}+\mathrm{dT}^{3}, \mathrm{~kJ} / \mathrm{k} \text { mol. } \mathrm{K} .
$$

| Gas | a | $\mathrm{b} \times 10^{3}$ | $\mathrm{c} \times 10^{6}$ | $\mathrm{~d} \times 10^{9}$ |
| :---: | :---: | :---: | :---: | :---: |
| $\mathrm{~N}_{2}$ | 29.5909 | -5.41 | 13.1829 | -4.968 |
| $\mathrm{H}_{2}$ | 28.6105 | 1.0194 | -0.1476 | 0.769 |

(iii) In one case, 26.6 lit of $\mathrm{NO}_{2}$ at $80 \mathrm{kPa} \& 298^{\circ} \mathrm{K}$ is allowed to stand until the equilibrium is reached. At equilibrium, the pressure is found to be 66.662 kPa . Calculate the partial pressure of $\mathrm{N}_{2} \mathrm{O}_{4}$ in the final mixture.

The reaction is $2 \mathrm{NO}_{2} \rightarrow \mathrm{~N}_{2} \mathrm{O}_{4}$.

## 4. Attempt any TWO of the following :

(i) The waste acid from a nitrating process contains $30 \% \mathrm{H}_{2} \mathrm{SO}_{4}, 35 \% \mathrm{HNO}_{3}$ \& $35 \% \mathrm{H}_{2} \mathrm{O}$ by weight. The acid is to be concentrated to contain $39 \% \mathrm{H}_{2} \mathrm{SO}_{4}$ \& $42 \% \mathrm{HNO}_{3}$ by adding conc. $\mathrm{H}_{2} \mathrm{SO}_{4}$ acid containing $98 \% \mathrm{H}_{2} \mathrm{SO}_{4}$ and conc. $\mathrm{HNO}_{3}$ acid containing $72 \% \mathrm{HNO}_{3}$ (by weight).

Calculate the quantities of acids to be mixed to get 1000 kg of desired mixed acid.
(ii) A feed containing 60 mole $\% \mathrm{~A}, 30$ mole $\% \mathrm{~B} \& 10$ mole $\%$ inerts enters a reactor. The product stream leaving the reactor is found to contain 2 mole $\%$ A. The reaction taking place is $2 \mathrm{~A}+\mathrm{B} \rightarrow \mathrm{C}$.

Find the percentage of original ' A ' getting converted to ' C '.
(iii) $10,000 \mathrm{~kg} / \mathrm{hr}$ of feed containing $20 \%$ methanol is continuously fed to a distillation column. Distillate is found to contain $98 \%$ methanol and waste solution (bottom product) contains $1 \%$ methanol. All percentages are by weight. Calculate : (a) mass flow rates of top \& bottom product. (b) Percent loss of methanol.
5. Attempt any TWO of the following :
(i) Centrifuge is fed with a slurry containing $25 \%$ solid by weight and wet solid obtained after drying is found to contain $8 \%$ moisture by weight and filtrate is found to contain 200 PPm solids.

If centrifuge machine produces $100 \mathrm{~kg} / \mathrm{h}$ desired wet product and quantity of slurry to be handled is 5000 kg per batch. Calculate : (i) time required for filteration, (ii) Loss of solids in filtrate per batch.
(ii) Pure sulphur is burnt in a sulphur burner with dry air. Oxygen is used $20 \%$ excess for complete combustion of sulphur to $\mathrm{SO}_{3}$. The efficiency of burner is such that only. $30 \%$ sulphur is converted to $\mathrm{SO}_{3}$ and remaining to $\mathrm{SO}_{2}$. Calculate (a) Composition of gases leavning the burner, (b) The weight of gas per kg of sulphur burnt.

> P.T.O.
(iii) Calculate the heat that must be removed in cooling 32 kg of oxygen from $488^{\circ} \mathrm{K}$ to $313{ }^{\circ} \mathrm{K}$. Using $\mathrm{Cp}^{\circ}$ data.

$$
\mathrm{Cp}^{\circ}=\mathrm{a}+\mathrm{bT}+\mathrm{cT}^{2}+\mathrm{dT}^{3} \mathrm{~kJ} /\left(\text { kmol. }{ }^{\circ} \mathrm{K}\right)
$$

| Gas | a | $\mathrm{b} \times 10^{3}$ | $\mathrm{c} \times 10^{6}$ | $\mathrm{~d} \times 10^{9}$ |
| :---: | :---: | :---: | :---: | :---: |
| $\mathrm{O}_{2}$ | 26.0257 | 11.7551 | -2.3426 | -0.5623 |

## 6. Attempt any FOUR of the following :

(i) Calculate the change in enthalpy between reactants and products if both are at $298 \mathrm{~K} \&$ if 5 mol of $\mathrm{C}_{2} \mathrm{H}_{4} \mathrm{O}$ is produced as per following reaction

$$
\mathrm{C}_{2} \mathrm{H}_{4}(\mathrm{~g})+\frac{1}{2} \mathrm{O}_{2}(\mathrm{~g}) \rightarrow \mathrm{C}_{2} \mathrm{H}_{4} \mathrm{O}(\mathrm{~g})
$$

Data :

| Component | $\Delta \mathrm{H}_{\mathrm{f}}^{\circ}, \mathrm{kJ} / \mathrm{mol}$ at 298 K |
| :---: | :---: |
| $\mathrm{C}_{2} \mathrm{H}_{4}(\mathrm{~g})$ | 52.50 |
| $\mathrm{C}_{2} \mathrm{H}_{4} \mathrm{O}(\mathrm{g})$ | -52.63 |

(ii) A natural gas has the following composition by volume. $\mathrm{CH}_{4}-82 \%$, $\mathrm{C}_{2} \mathrm{H}_{6}-12 \%$ \& $\mathrm{N}_{2}-6 \%$. Calculate the density of gas at $288 \mathrm{k} \& 101.325 \mathrm{kPa}$.
(iii) The $\mathrm{NH}_{3}$ - air mixture containing 0.2 kg NH 3 per kg air, enters into absorption system where $\mathrm{NH}_{3}$ is absorbed in water. The gases leaving the system is found to contain $0.004 \mathrm{~kg} \mathrm{NH}_{3}$ per kg of air. Calculate the percentage recovery of $\mathrm{NH}_{3}$.
(iv) Ethylene oxide is produced by oxidation of ethylene. 100 kmol of ethylene is fed to reactor and product contains 80 kmol of ethylene oxide \& 10 kmol of $\mathrm{CO}_{2}$. Calculate $\%$ conversion of ethylene \& \% yield of ethylene oxide.
(v) 100 kmol of ethanol are charged to dehydrogenation reactor to produce acetaldehyde. The product stream contains 45 kmol acetaldehyde. Calculate percent conversion of ethanol.
(vi) A wet lumber containing $5 \% \mathrm{H}_{2} \mathrm{O}$, is dried to $1 \%$ water in a hot air dryer. Air containing $0.5 \mathrm{wt} \%$ water is fed to the dryer. The moist air leaving the dryer contains $2 \%$ water. Calculate the air required to dry $2000 \mathrm{~kg} / \mathrm{h}$ of wet lumber.

