## 23124 <br> 3 Hours / 70 Marks

Seat No. $\square$

Instructions : (1) All Questions are compulsory.
(2) Figures to the right indicate full marks.
(3) Assume suitable data, if necessary.

## Marks

1. Attempt any FIVE of the following :
(a) Give the SI unit of force \& energy.
(b) What are products of complete and incomplete combustion?
(c) Draw the block diagram of distillation unit showing all input and output.
(d) Define : (i) Limiting component (ii) Excess component
(e) Define: (i) Partial pressure (ii) Pure component volume
(f) Calculate the volume occupied by 20 kg of chlorine gas at a pressure of 100 KPa and 298 K .
(g) Name any two each of fundamental quantity and derived quantity.
2. Attempt any THREE of the following :
(a) State Dalton's law and Amagat's law. Give their mathematical equations.
(b) Ammonia is produced by the following reaction : $\mathrm{N}_{2}+3 \mathrm{H}_{2} \rightarrow 2 \mathrm{NH}_{3}$ Calculate :
(i) Molal flow rate of hydrogen corresponding to nitrogen. Feed rate of 25 $\mathrm{k}_{\mathrm{mol}} / \mathrm{h}$, if they are fed in the stoichiometric proportions.
(ii) Kg of $\mathrm{NH}_{3}$ produced per hour if conversion is $25 \%$ and nitrogen feed rate is $25 \mathrm{k}_{\mathrm{mol}} / \mathrm{h}$.
(c) An evaporator is fed with $15000 \mathrm{~kg} / \mathrm{h}$ of a solution containing $10 \% \mathrm{NaCl}$, $15 \% \mathrm{NaOH}$ and rest water. In the operation, water is evaporated and NaCl is precipitated as crystals. The thick liquor leaving the evaporator contains $45 \%$ $\mathrm{NaOH}, 2 \% \mathrm{NaCl}$ and rest water.
(i) Draw the detail block diagram of this operation.
(ii) Calculate $\mathrm{kg} / \mathrm{h}$. of thick liquor
(d) Explain different types of fuels with example.
3. Attempt any THREE of the following :
(a) Define :
(i) Yield
(ii) Conversion
(iii) Selectivity
(iv) Stoichiometric ratio
(b) State \& explain Hess's law of constant heat summation.
(c) Convert following pressure values in KPa .
(i) 100 mm of Hg
(ii) 2 atm
(d) In the production of Sulphur trioxide, $100 \mathrm{k}_{\mathrm{mol}}$ of $\mathrm{SO}_{2}$ and $100 \mathrm{k}_{\mathrm{mol}}$ of $\mathrm{O}_{2}$ are fed to a reactor. If the percent conversion of $\mathrm{SO}_{2}$ is 80 , calculate the composition of product stream on mole basis.
4. Attempt any THREE of the following :
(a) Define:
(i) Sensible heat
(ii) Latent heat
(iii) Specific heat
(iv) Heat of reaction
(b) 2000 kg of wet solids containing $70 \%$, solid by weight are fed to a tray dryer where it is dried by hot air. The product finally obtained is found to contain $1 \%$ moisture by weight.

Calculate :
(i) Kg of water removed
(ii) Kg of dried product obtained
(c) Explain bypass \& recycle operation with block diagram.
(d) Define gross and net calorific value.
(e) Convert the following :
(i) $1000 \mathrm{~kg} / \mathrm{m}^{3}$ into gram $/ \mathrm{cm}^{3}$
(ii) $10 \mathrm{~m}^{3} / \mathrm{hr}$. into lit/sec.
5. Attempt any TWO of the following :
(a) A natural gas has the following composition by volume
$\mathrm{CH}_{4}-82 \%, \mathrm{C}_{2} \mathrm{H}_{6}-12 \% \& \mathrm{~N}_{2}-6 \%$
Calculate :
(i) Density of gas at 288 K and 101.325 KPa
(ii) Composition in weight percent
(b) Soyabean seeds are extracted with hexane in batch extractor. The flaked seeds are found to contain $18.6 \%$ oil, $69 \%$ solid and $12.4 \%$ moisture. At the end of process, cake is separated from hexane - oil mixture.

The cake is analysed to contain $0.8 \%$ oil, $87.7 \%$ solid and $11.5 \%$ moisture (by weight).

Calculate the percentage recovery of oil.
(c) $\mathrm{C}_{2} \mathrm{H}_{4} \mathrm{O}$ is prepared by oxidation of $\mathrm{C}_{2} \mathrm{H}_{4}, 100 \mathrm{k}_{\mathrm{mol}}$ of $\mathrm{C}_{2} \mathrm{H}_{4}$ and $100 \mathrm{k}_{\mathrm{mol}}$ of $\mathrm{O}_{2}$ are fed to a reactor. The conversion of $\mathrm{C}_{2} \mathrm{H}_{4}$ is $85 \%$ and yield of $\mathrm{C}_{2} \mathrm{H}_{4} \mathrm{O}$ is
$94.12 \%$. The reactions taking place are
$\mathrm{C}_{2} \mathrm{H}_{4}+1 / 2 \mathrm{O}_{2} \rightarrow \mathrm{C}_{2} \mathrm{H}_{4} \mathrm{O}$
$\mathrm{C}_{2} \mathrm{H}_{4}+3 \mathrm{O}_{2} \rightarrow 2 \mathrm{CO}_{2}+2 \mathrm{H}_{2} \mathrm{O}$
Calculate the composition of product stream leaving the reactor.
6. Attempt any TWO of the following :
(a) Pure ethylene is heated from 303 k to 523 k at atmospheric pressure.

Calculate the heat added per $\mathrm{k}_{\mathrm{mol}}$ of ethylene using heat capacity data given below.

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\begin{aligned}
\mathrm{C}_{\mathrm{p}}^{\circ}= & 4.1261+155.0213 \times 10^{-3} \mathrm{~T}-81.5455 \times 10^{-6} \mathrm{~T}^{2} \\
& +16.9755 \times 10^{-9} \mathrm{~T}^{3}
\end{aligned}
$$

(b) A combustion reactor is fed with $50 \mathrm{k}_{\mathrm{mol}} / \mathrm{h}$ of butane and $2000 \mathrm{k}_{\mathrm{mol}} / \mathrm{h}$ of air. Calculate \% excess air used and composition of the gases leaving reactor, assuming complete combustion of butane.
(c) The waste acid from nitrating process containing $20 \% \mathrm{HNO}_{3}, 55 \% \mathrm{H}_{2} \mathrm{SO}_{4}$ \& $25 \% \mathrm{H}_{2} \mathrm{O}$ by weight is to be concentrated by addition of concentrated $\mathrm{H}_{2} \mathrm{SO}_{4}$ acid containing $95 \% \mathrm{H}_{2} \mathrm{SO}_{4}$ and concentrated $\mathrm{HNO}_{3}$ acid containing $90 \%$ $\mathrm{HNO}_{3}$ to get desired mixed acid containing $26 \% \mathrm{HNO}_{3} \& 60 \% \mathrm{H}_{2} \mathrm{SO}_{4}$.
Calculate quantities of waste and concentrated acids required to get 1000 kg of desired mixed acid.

